

# Ciências ULisboa

Faculdade  
de Ciências  
da Universidade  
de Lisboa

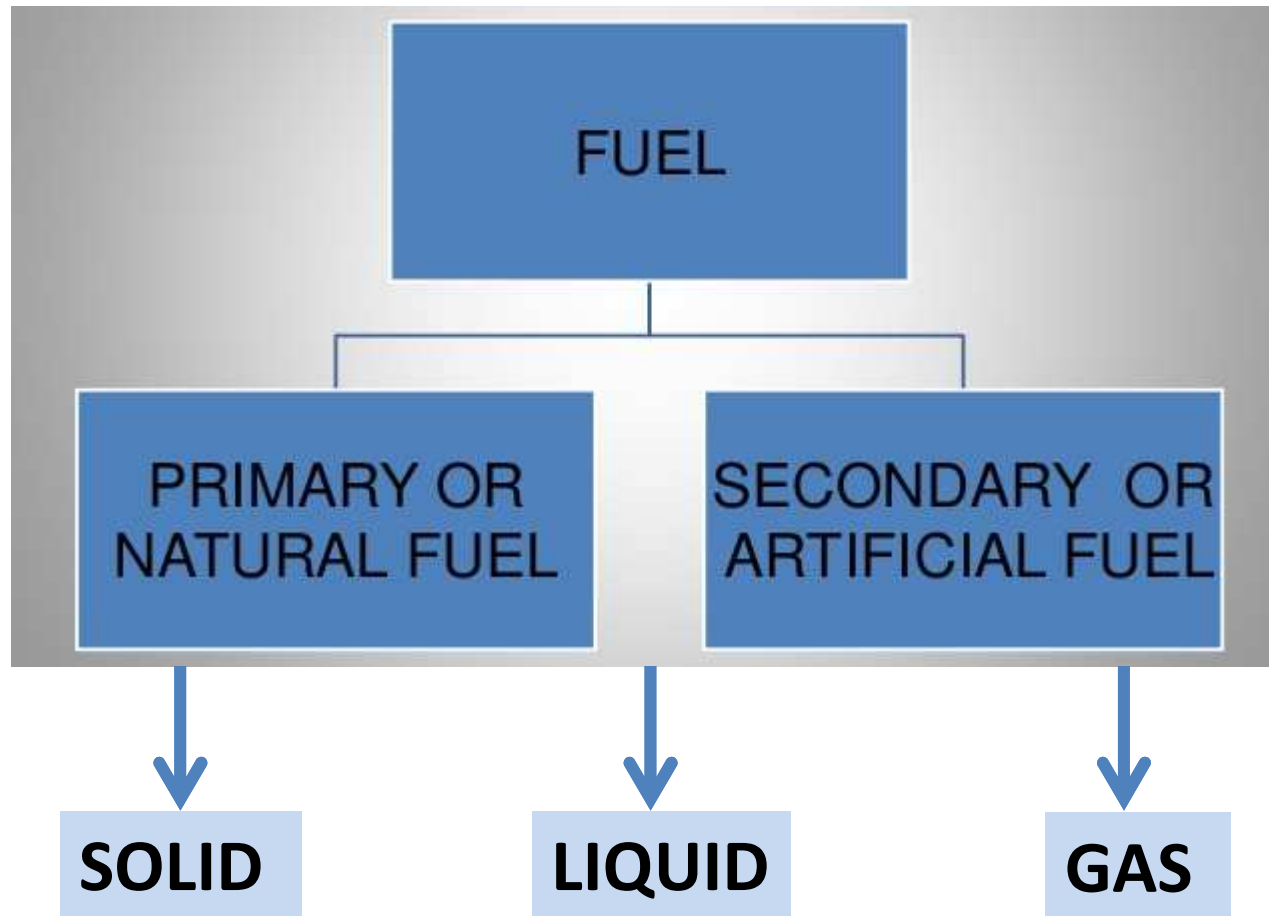
**DISCIPLINA MIEA 2019**

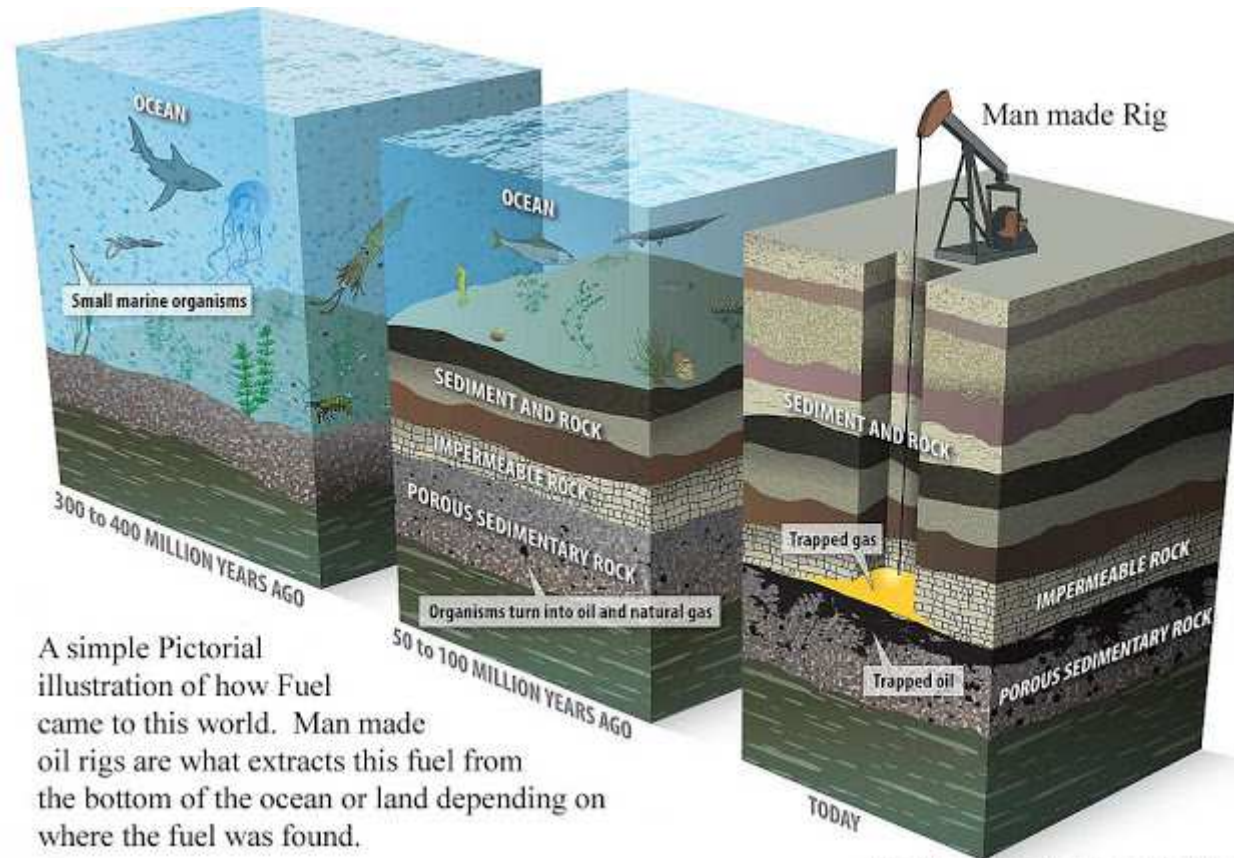


# **Technologies of combustion**

## Corpo docente

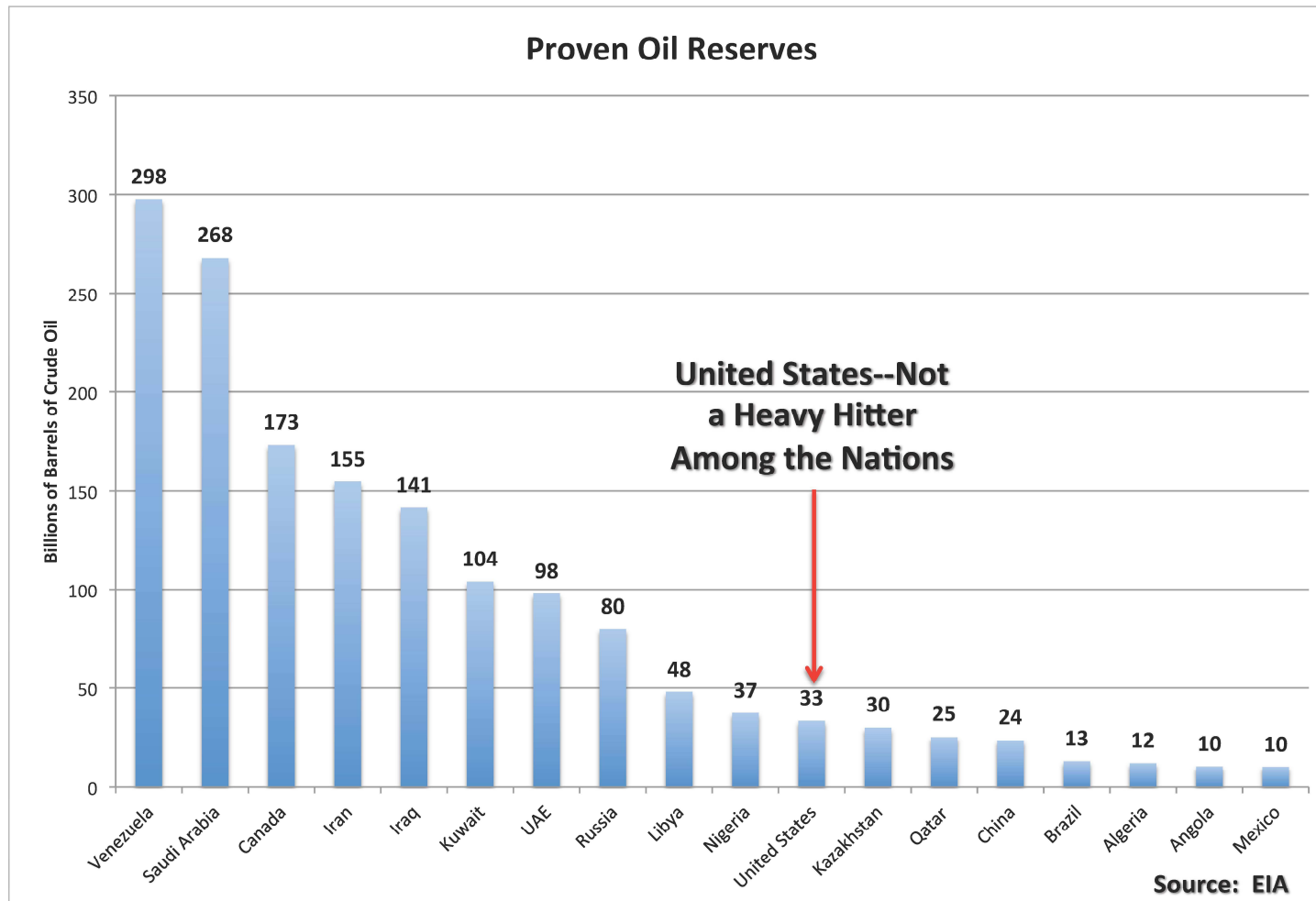
**Carla Silva (Teóricas e práticas) /Theory and practice**  
**[camsilva@ciencias.ulisboa.pt](mailto:camsilva@ciencias.ulisboa.pt)**

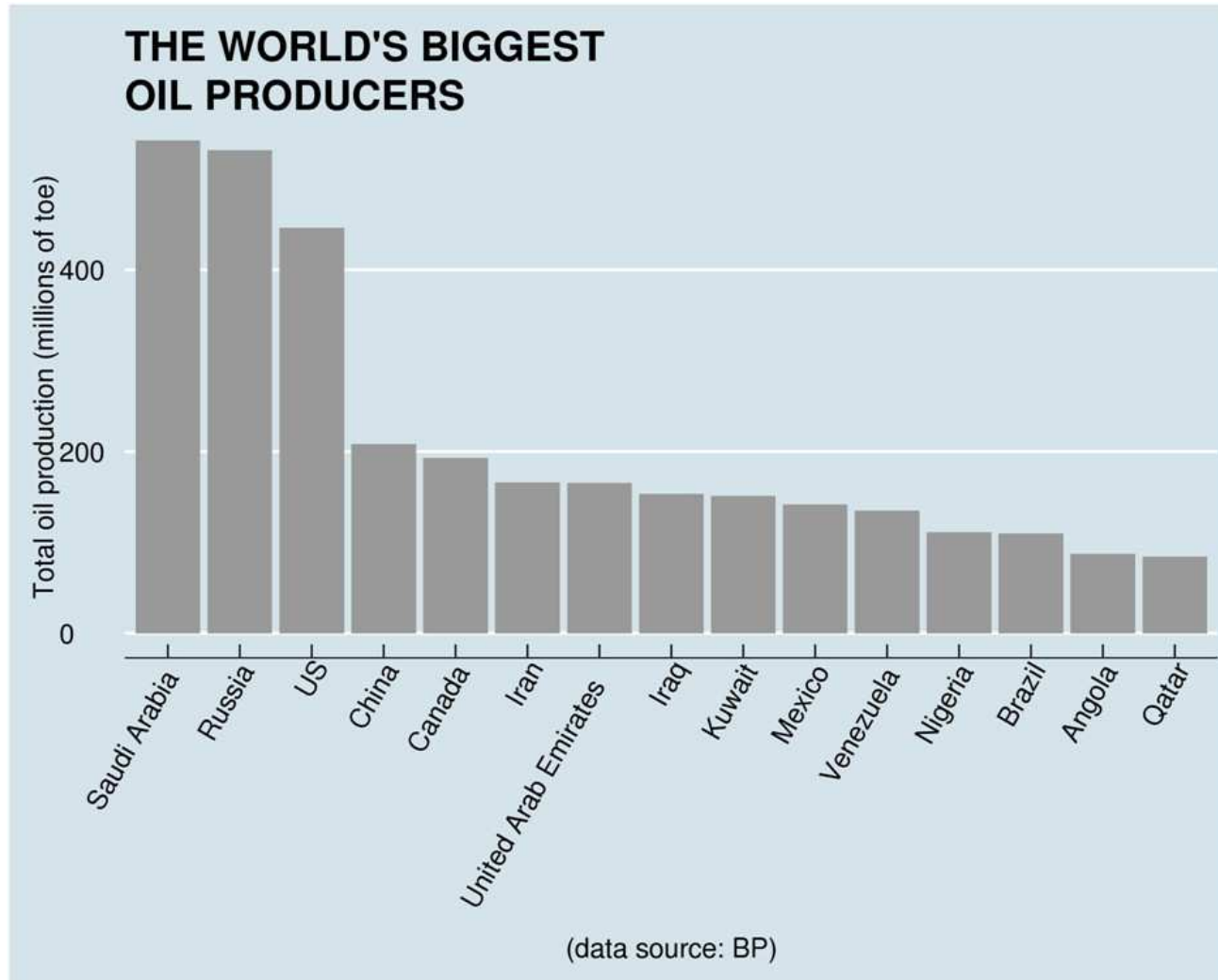




A simple Pictorial illustration of how Fuel came to this world. Man made oil rigs are what extracts this fuel from the bottom of the ocean or land depending on where the fuel was found.

This picture is taken from timmeko's photostream





## Capacity:

**220 thousand  
Barrel a day ~  
26 million  
litters**

## Sines refinery Portugal

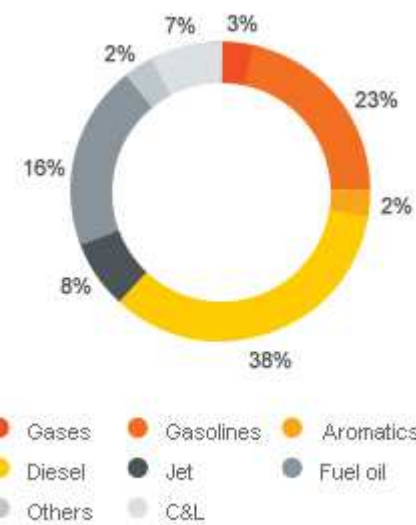


## Matosinhos refinery Portugal

**110 thousand  
Barrel a day ~  
13 million  
litters**

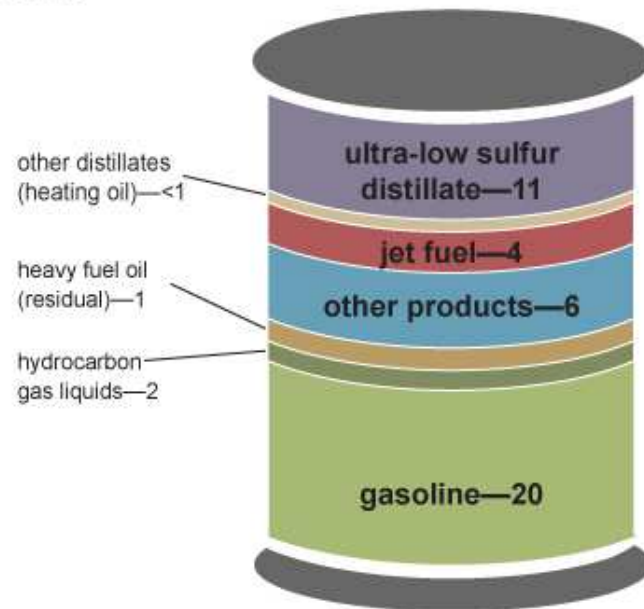
## Installed capacity:

330 barrels a day



## Petroleum products made from a barrel of crude oil, 2016

volumes



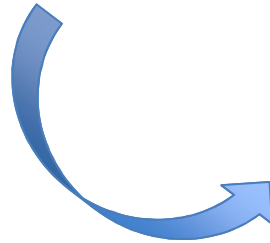
Note: A 42-gallon (U.S.) barrel of crude oil yields about 45 gallons of petroleum products because of refinery processing gain. The sum of the product amounts in the image may not equal 45 because of independent rounding.

Source: U.S. Energy Information Administration, *Petroleum Supply Monthly*, February 2017, preliminary data for 2016

- Liquefied petroleum gas
- Gasoline
- Naphtha
- Jet/kerosene
- Diesel
- Fuels
- Base oils
- Lubricating oils
- Paraffin
- Aliphatic solvents and aromatics, benzene, toluene and xylenes
- Bitumen

100% imported.....

Brazil, Angola, Saudi Arabia, Algeria, Cameroon and Equatorial Guinea



**Portuguese refinery**





**Direção Geral de Energia e Geologia**  
 Direção de Serviços de Planeamento Energético e Estatística

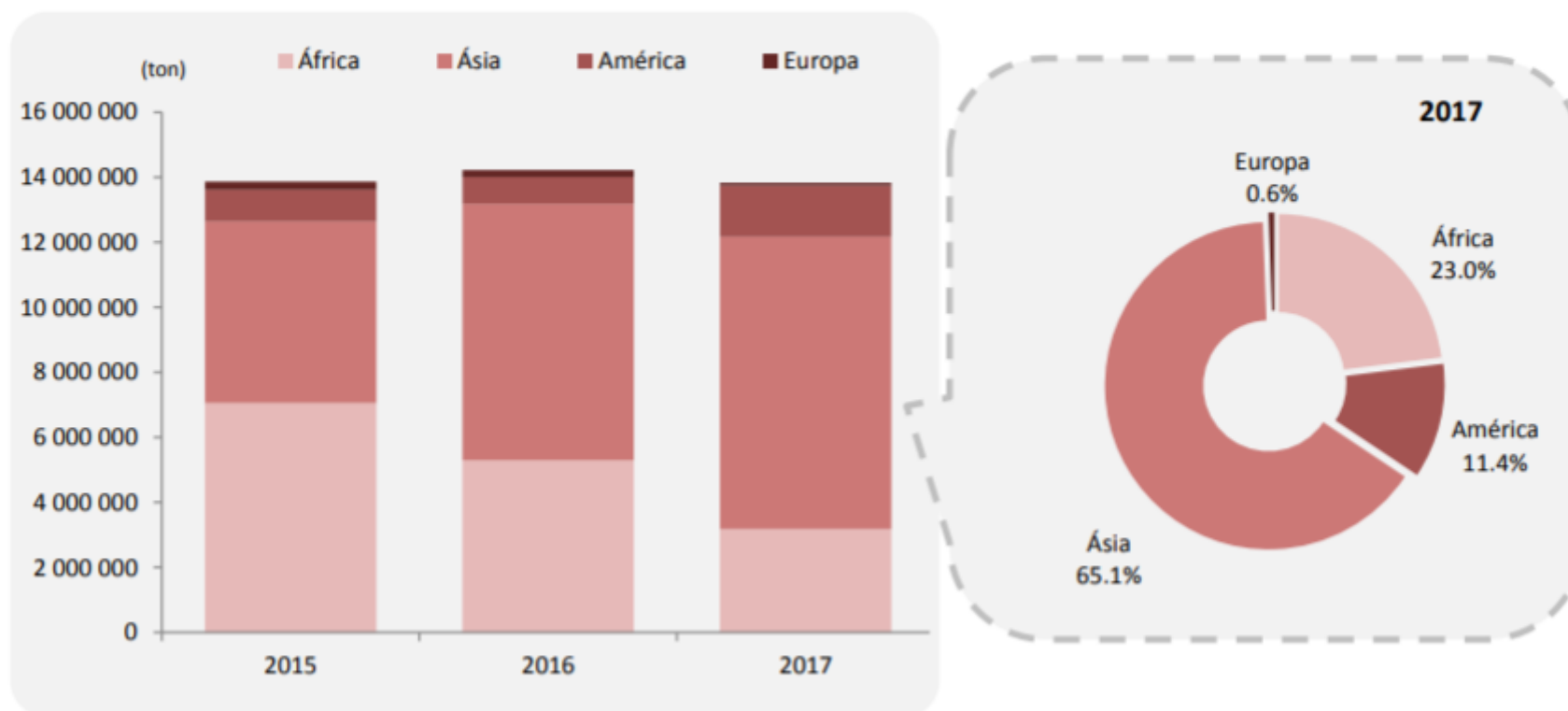
**IMPORTAÇÕES DE PRODUTOS DO PETRÓLEO E BIOCOMBUSTÍVEIS EM 2015**  
 (toneladas)

País	Produtos Intermediários	Produtos Energéticos											Produtos Não Energéticos					Total	
		GPL	Gasolina	AV. Gas	Jets	Gasóleo	Petróleos	Fuel	Coque	Bio diesel <sup>1</sup>	Bio gasolina <sup>2</sup>	Sub-Total	Nafta	Lubrificantes	Asfaltos	Parafinas	Solventes		Sub-Total
Alemanha		165	30			3						198		1.357			7	1.364	1.562
Argélia		22.808										22.808							22.808
Bélgica	161.632	834	5.574			20.378						188.418		2.462				2.462	190.880
Dinamarca		4.116										4.116							4.116
E.U.A.		128.182						231.220				359.402							359.402
Espanha	27.099	245.549	111.281	490	10.512	702.789	907	71.177	157.097		10.383	1.326.871	61.034	29.598	124.379	4.599	106	219.716	1.546.587
França	86.804	8.190		530							33.114	95.524		8.220			10	8.230	103.754
Grécia								29.924				29.924							29.924
Guiné		9.000										9.000							9.000
Guiné Equatorial		17.264										17,264							17,264
Holanda	76.979	5.606	19.905			20.495		171.819		24.201	15.565	319.095		45				45	319.140
Itália														81				81	81
Letónia						20.424						20.424							20.424
Noruega		106.308										106.308							106.308
Reino Unido		93.974		494		1						94.469		893				893	95.362
República do Congo		49.586										49.586							49.586
República Dominicana		49.454										49.454							49.454
Rússia	789.597											789.597							789.597
Suécia		13.575										13.575							13.575
Suíça						18.171						18.171		6				4	18.177
País não especificado		6.215										6.215							6.215
<b>Total</b>	<b>1.161.901</b>	<b>741.126</b>	<b>136.790</b>	<b>1.484</b>	<b>10.512</b>	<b>782.261</b>	<b>907</b>	<b>272.920</b>	<b>388.317</b>	<b>30.538</b>	<b>65.400</b>	<b>3.526.787</b>	<b>61.034</b>	<b>42.662</b>	<b>124.379</b>	<b>4.899</b>	<b>123</b>	<b>232.797</b>	<b>3.759.554</b>

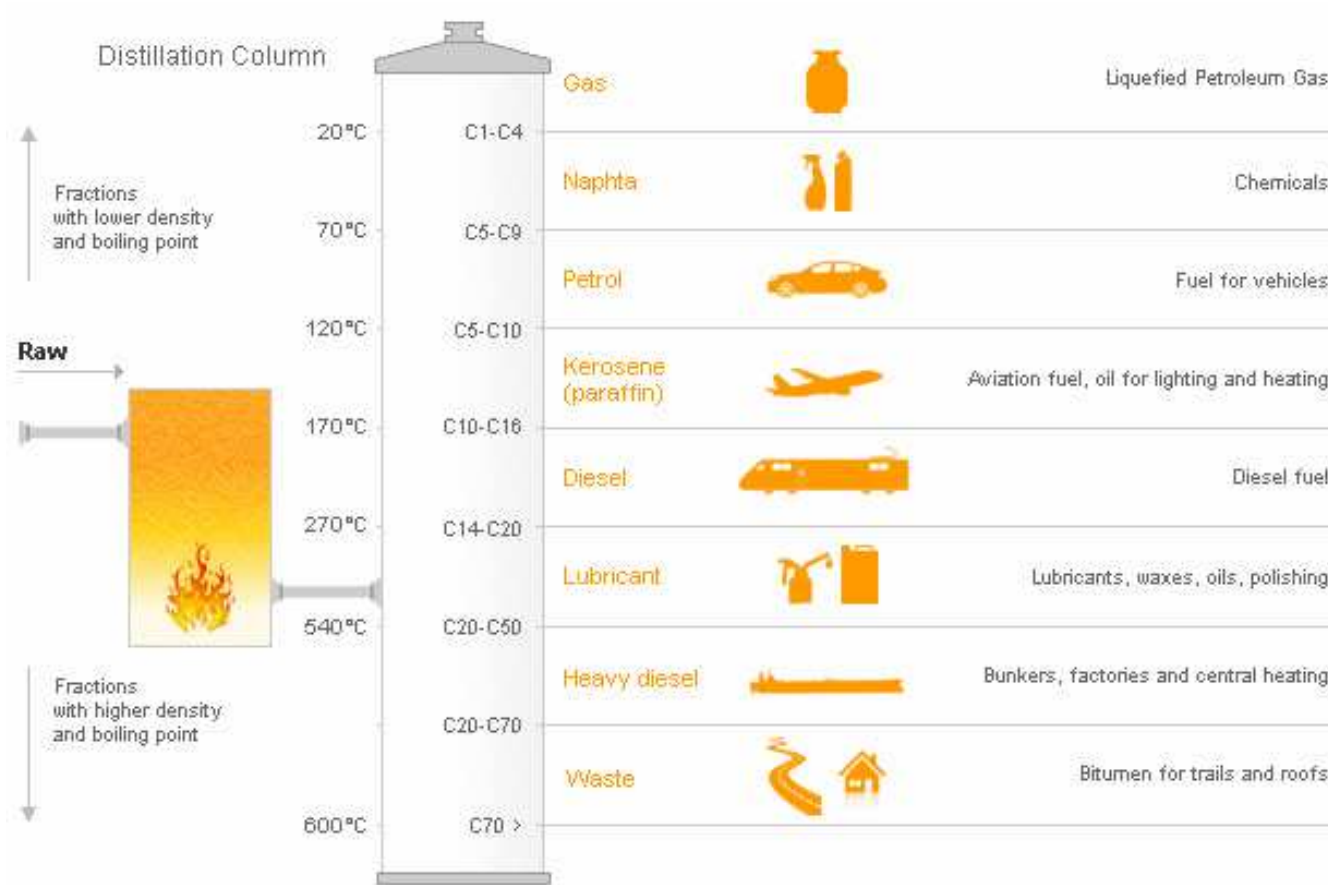
30-01-2017

Notas:  
 os dados são provisórios  
<sup>1</sup> inclui HVO  
<sup>2</sup> inclui bioetanol e bioETBE

Figura 3 - Estrutura do Petróleo Bruto Importado, por Origens (2015 a 2017)



Fonte: DGEG



<https://www.youtube.com/watch?v=o2xhmrpOtc>

## Liquid fuel properties

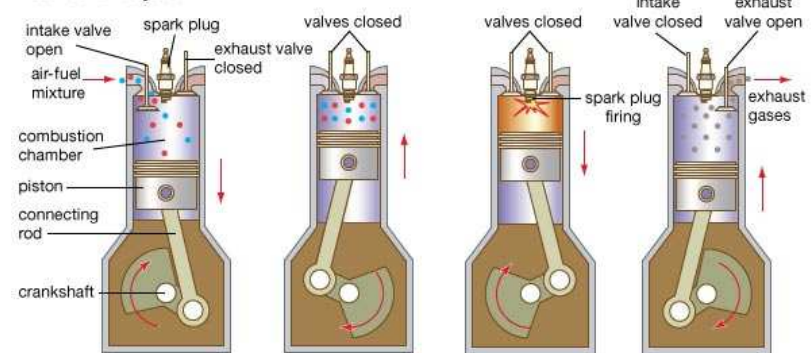
LPG (Propane) Properties Chart

LPG Boiling Point	-42 °C or -44 °F
LPG Melting - Freezing Point	-188 °C or -306.4 °F
Specific Gravity of Liquid LPG	0.495 (25°C)
LPG Gaseous Density	1.898 kg/m <sup>3</sup> (15°C) or 0.1162 lb/ft <sup>3</sup>
Energy Content of LPG	25 MJ/L or 91,547 BTU/Gal (60°F)
LPG Gaseous Expansion	1 L (liquid) = 0.27 M <sup>3</sup> (gas)
Flame Temperature	1967 °C or 3573 °F
Limits of Flammability	2.15% to 9.6% LPG/air
Autoignition Temperature	470 °C or 878 °F
Molecular Weight	44.097 kg/kmole

Note: Some numbers have been rounded.

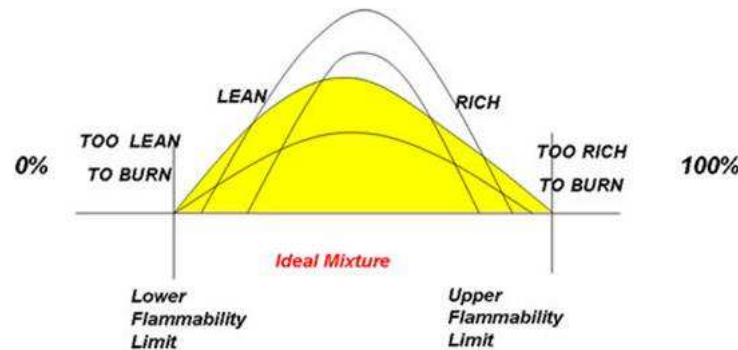
Octane number: ~ 110 (high resistance to autoignition)

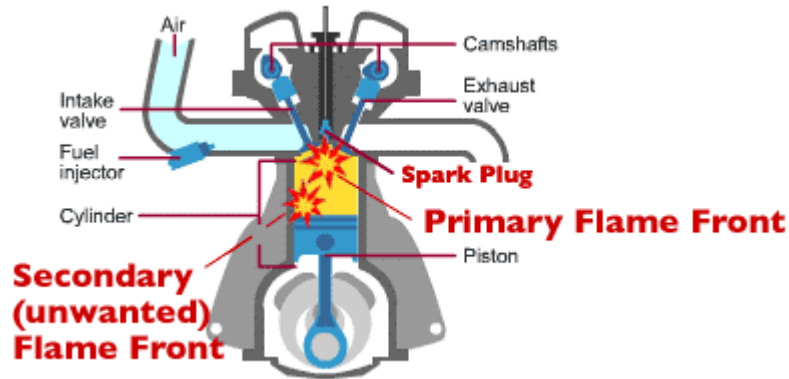
Four-stroke cycle



© 2007 Encyclopædia Britannica, Inc.

Limits flammability:



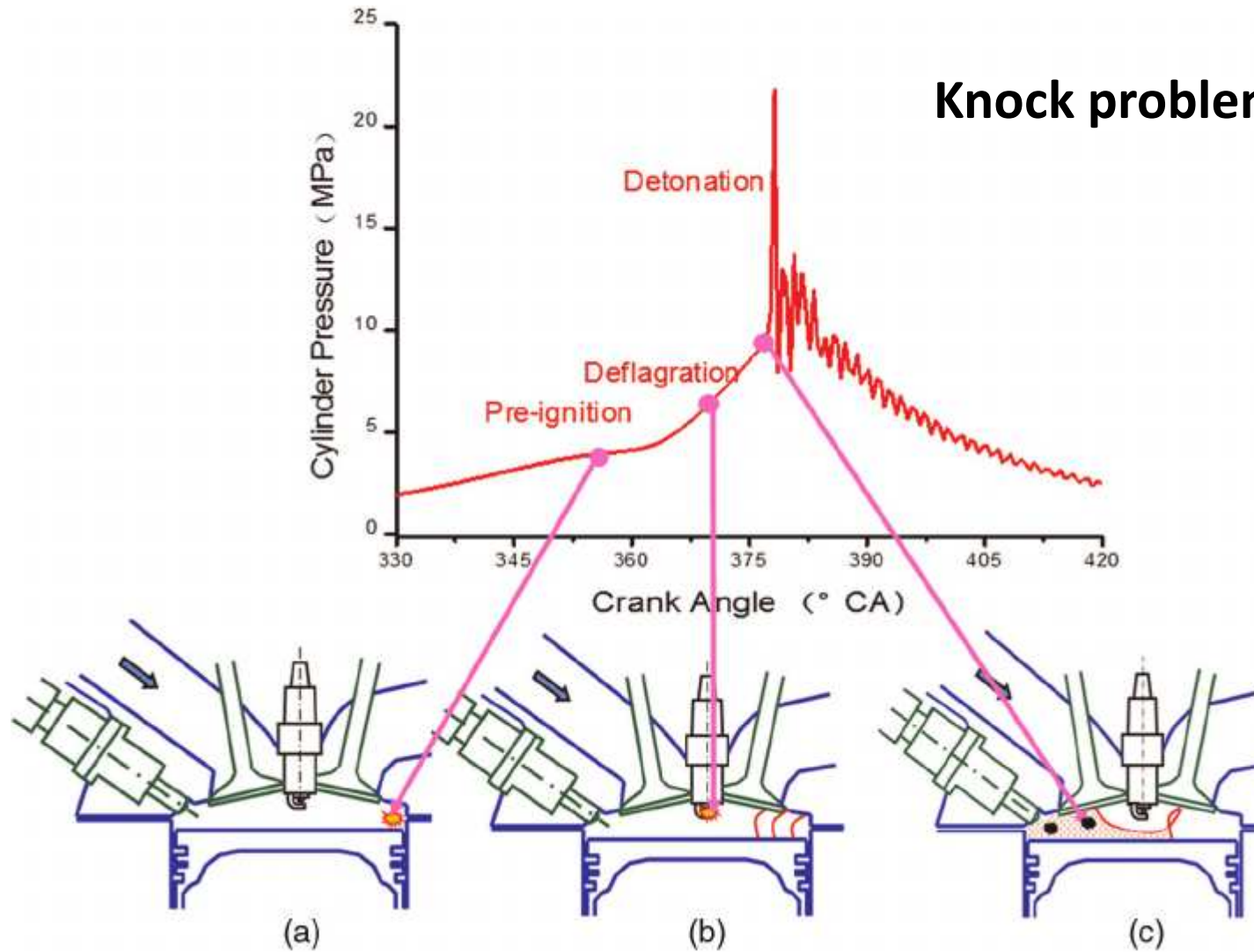


This photo of a badly damaged piston indicates the effects of long-term engine knock.

Octane number: ~ 110 (high resistance to autoignition)

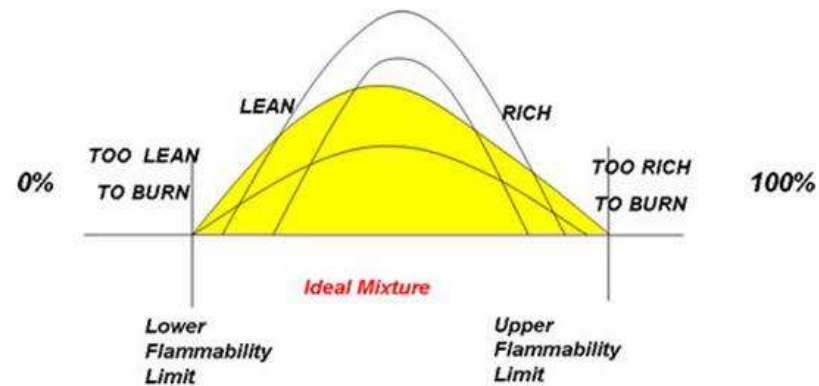


## Knock problem



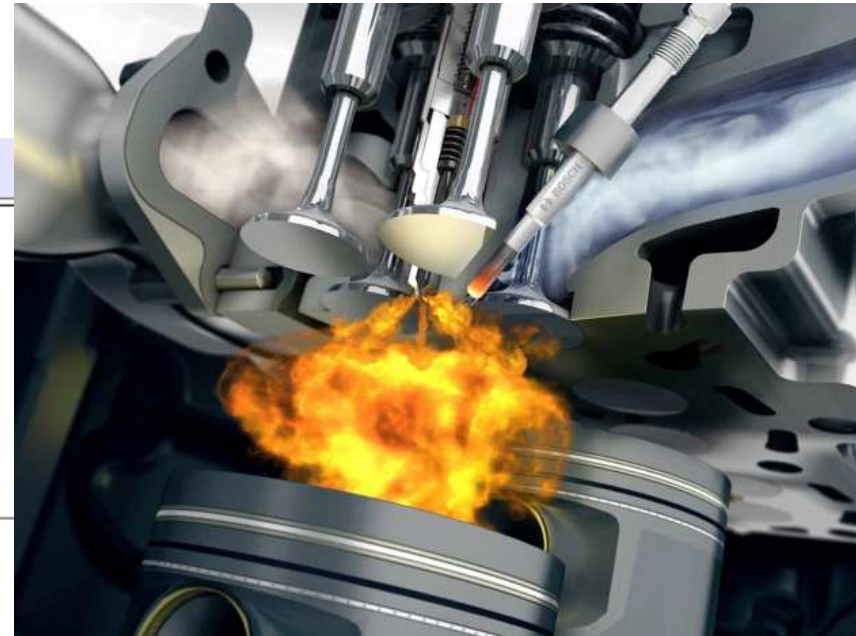
P#16 Calculate the (A/F)s of propane ( $C_3H_8$ ). What is the mass A/F for each limit of flammability?

Limits flammability:  
% volume in air




## Diesel

PHYSICAL PROPERTIES	
Boiling point: 282-338°C	←
Melting point: -30 - -18°C	
Density: 0.87-0.95 g/cm <sup>3</sup>	←
Solubility in water, g/100ml at 20°C: 0.0005	
Flash point: 52°C c.c.	
Auto-ignition temperature: 254-285°C	←
Explosive limits, vol% in air: 0.6-6.5	
Octanol/water partition coefficient as log Pow: >3.3	



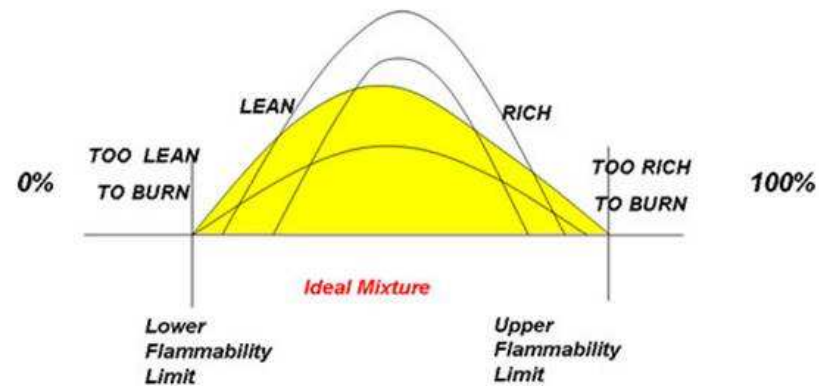
**Cetane number=45** (between **40..55**); **60..65** for biodiesel.

This is a measure of a fuel's ignition delay; the time period between the start of injection and start of combustion (ignition) of the fuel, with larger cetane numbers having **lower ignition delays**.


 Remember ignition delay effect on emissions!!!!  
 Higher NO<sub>x</sub> for biodiesel

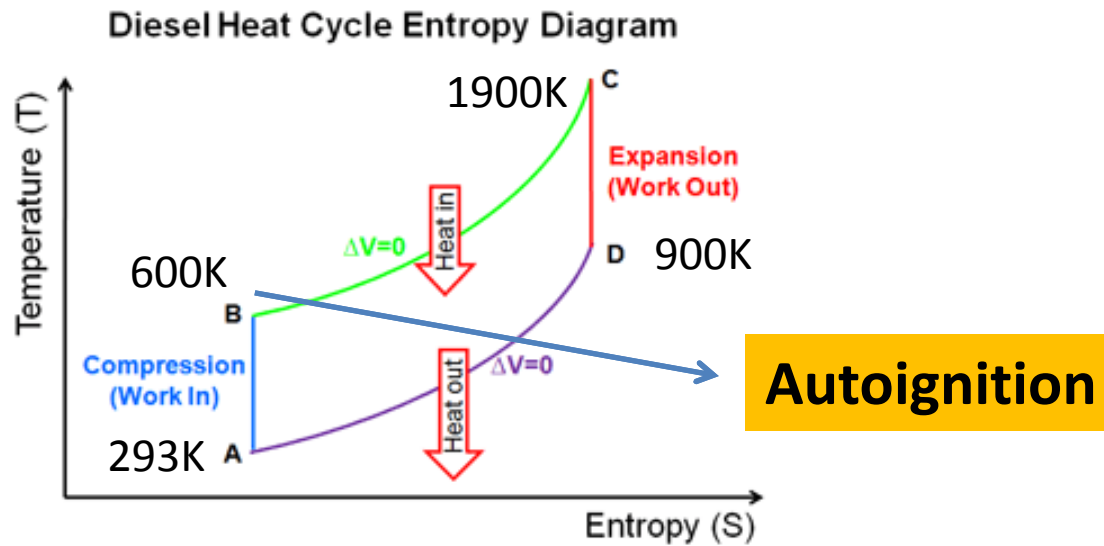
P#17 Calculate the (A/F)s of Diesel ( $C_7H_{14}$ ). What is the mass A/F for each limit of flammability?

Limits flammability:  
% volume in air



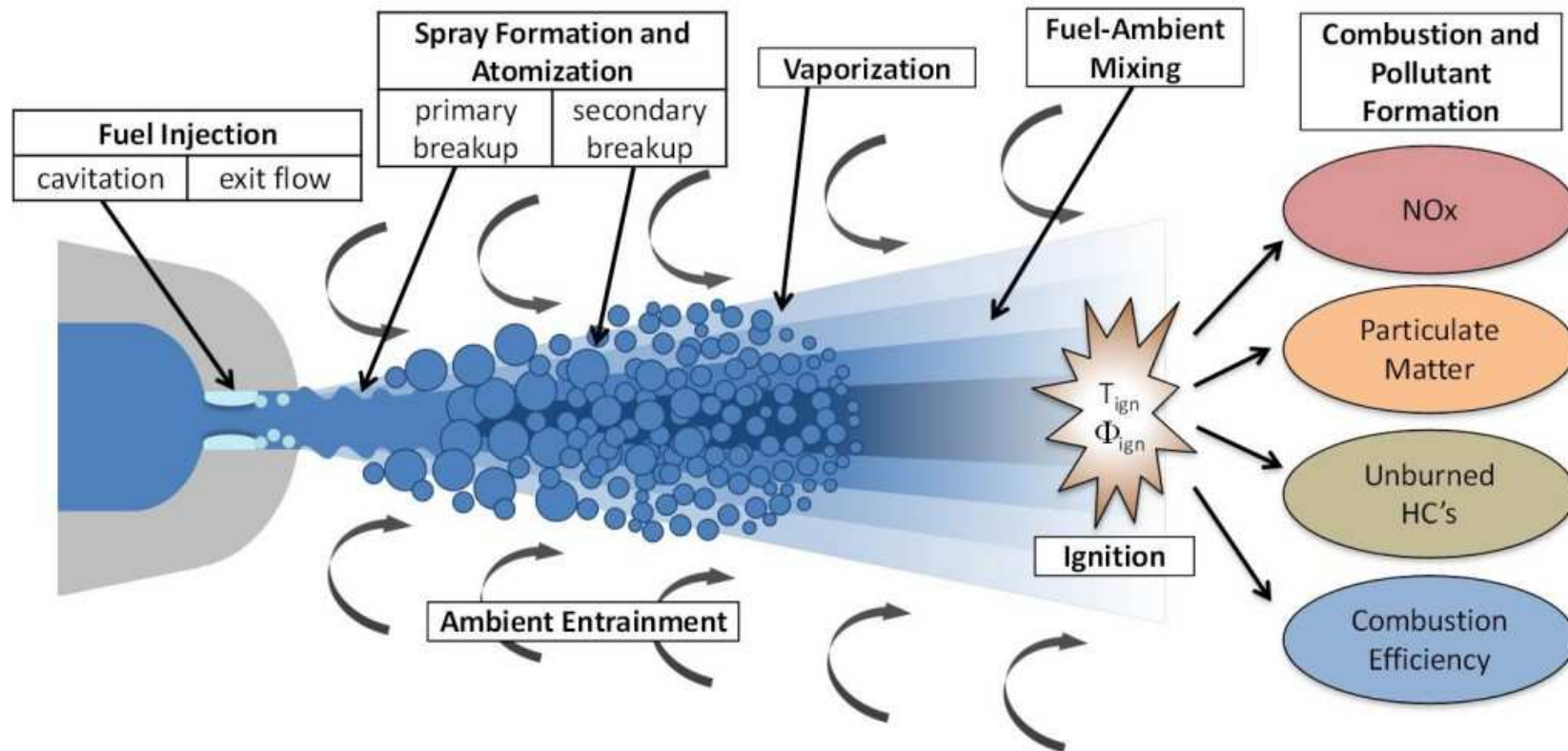
## Diesel AUTOIGNITION

Compression ratio =18



# Combustion of droplets

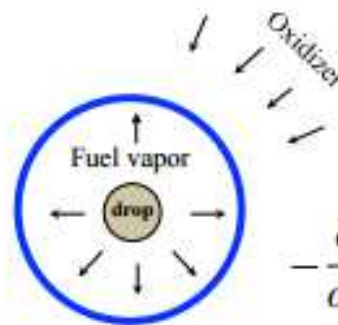
Droplets distribution range from few microns to around 500µm



## Droplet Vaporization and Combustion:

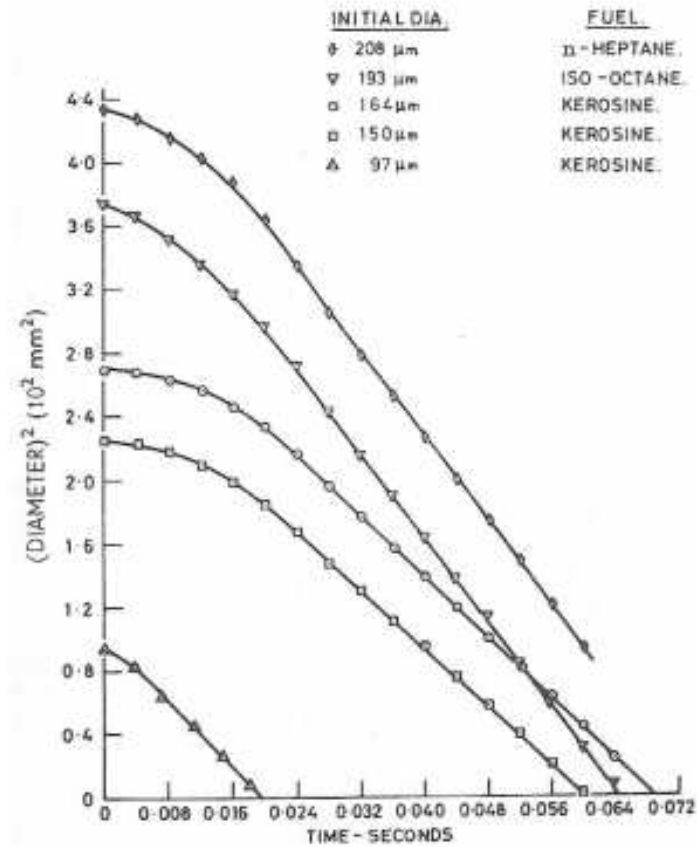
### Assumptions:

- droplet is a sphere
- single component fuel
- quiescent ambience
- no gravity
- spherical symmetry
- quasi-steady approximation
- one-step overall chemical reaction ( $F + O \rightarrow \text{Products}$ )



$$-\frac{d}{dt} \left( \frac{4}{3} \pi \rho_l r_s^3 \right) = \dot{m}$$

mass flow rate  
 mass per unit time leaving the droplet

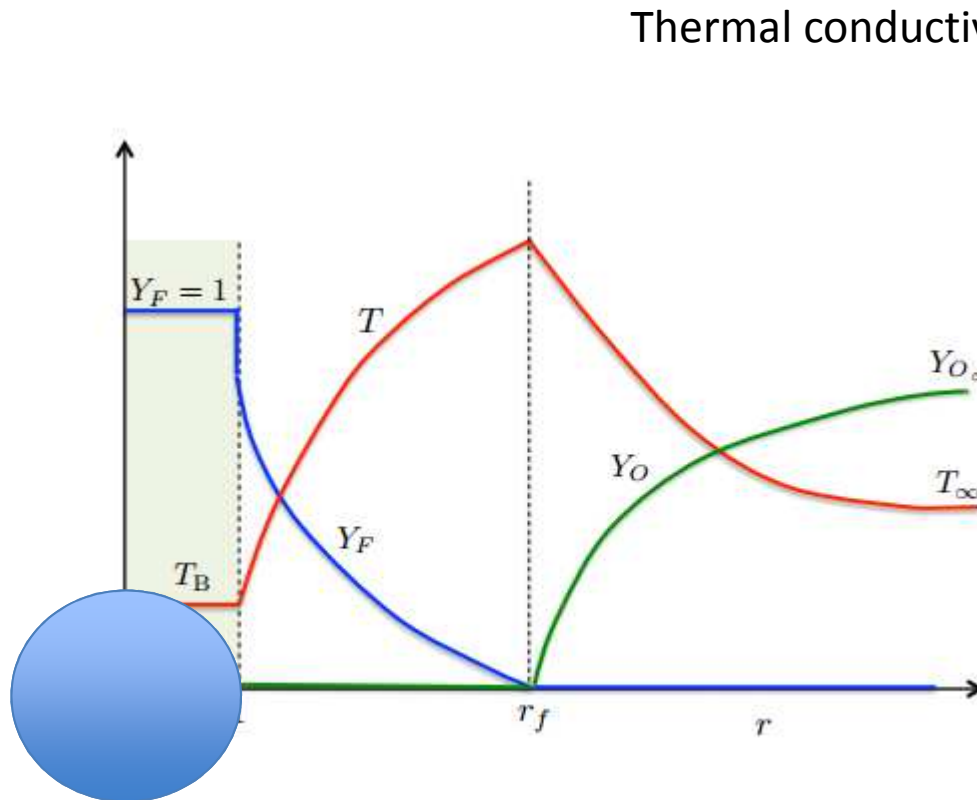


$D^2$  law

$$\text{Droplet lifetime} = \frac{D_0^2}{K}$$

$$K \sim 1 \times 10^{-6} \text{ m}^2/\text{s}$$

Nuruzzaman et al. PCI, 1971



Thermal conductivity

$$\dot{m}_{fu} = \frac{4\pi\lambda_g r_s}{c_{p,g}} \ln(B + 1)$$

Heat capacity

D<sup>2</sup> law

$$t_d = \frac{D_0^2}{K}$$

droplet diameter

droplet life time

$$B = \left( \frac{LHV \cdot y_{O_2, \infty}}{s} + c_{p,g} (T_{\infty} - T_s) \right) \frac{1}{h_{f,g}}$$

mO<sub>2</sub>/mfu stoichiometric

Heat of vaporization of the fuel

PROPERTIES AT AVERAGE FLAME  
 TEMPERATURE AND DROPLET BOILING  
 POINT TEMPERATURE

$$\bar{T} = \frac{T_s + T_f}{2}$$

$$c_{p,g} = c_{p,fu}(\bar{T})$$

$$\lambda_g = 0.4 \lambda_{fu}(\bar{T}) + 0.6 \lambda_{ox}(\bar{T})$$

$$B = \left( \frac{LHV \cdot y_{O_2,\infty}}{s} + c_{p,g} (T_\infty - T_s) \right) \frac{1}{h_{f,g}}$$

$\frac{1}{h_{f,g}}$  → Heat of vaporization of the fuel  
 $\frac{LHV \cdot y_{O_2,\infty}}{s}$  → mO<sub>2</sub>/mfu stoichiometric

Thermal conductivity

$$\dot{m}_{fu} = \frac{4\pi\lambda_g r_s}{c_{p,g}} \ln(B + 1)$$

Heat capacity

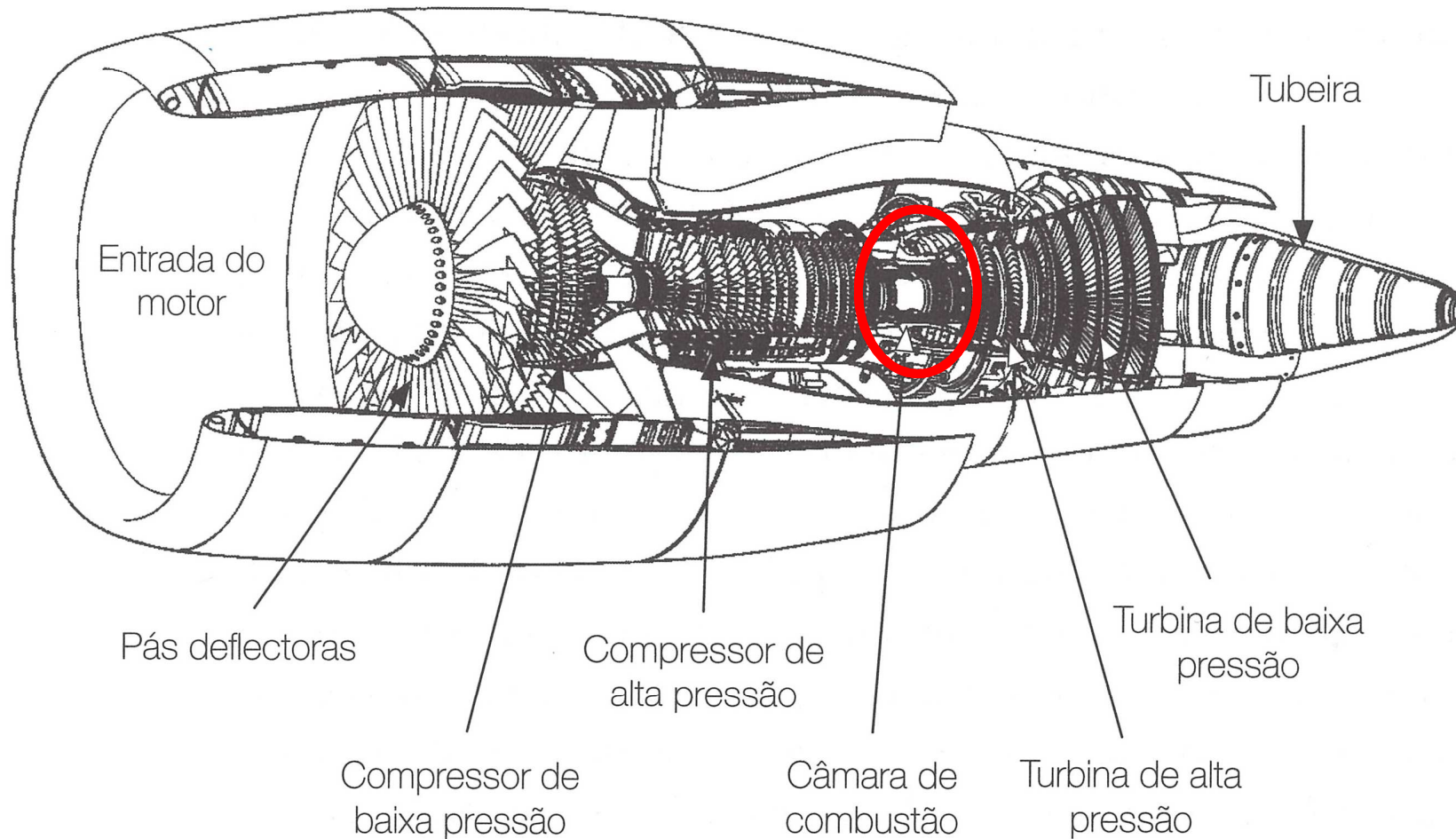
D<sup>2</sup> law

$$t_d = \frac{D_0^2}{K}$$

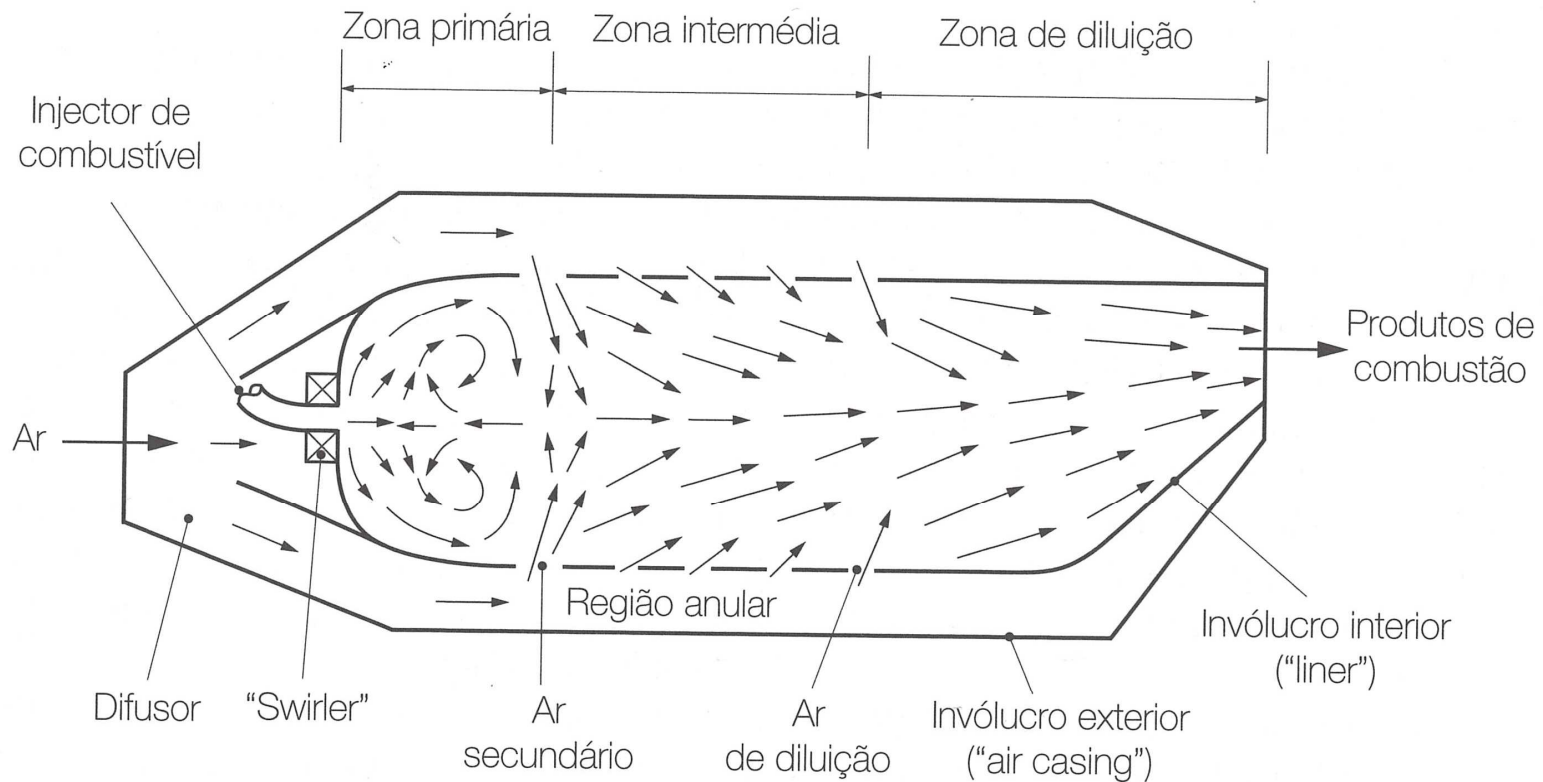
droplet diameter

droplet life time

Turbina a gás de um avião.

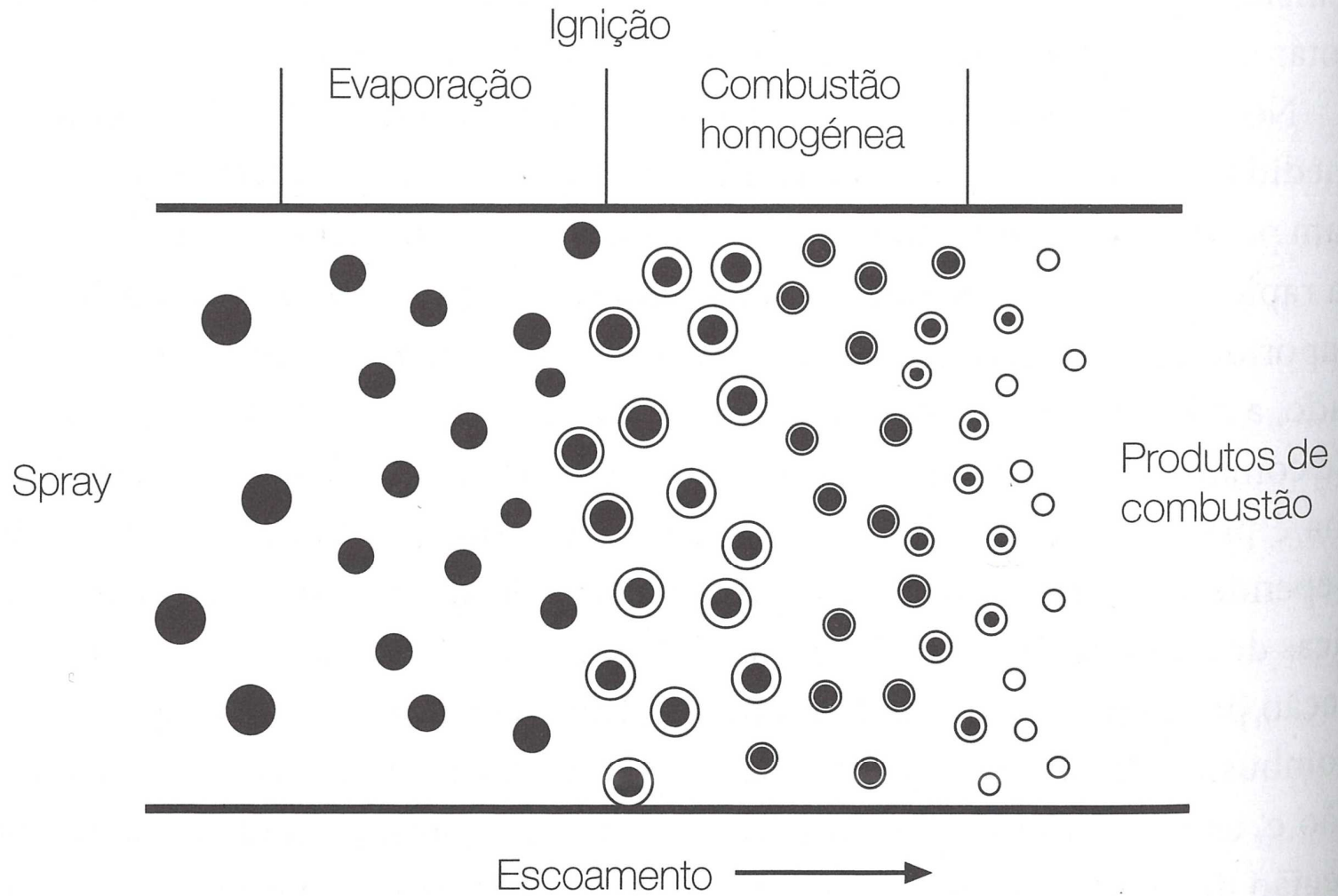


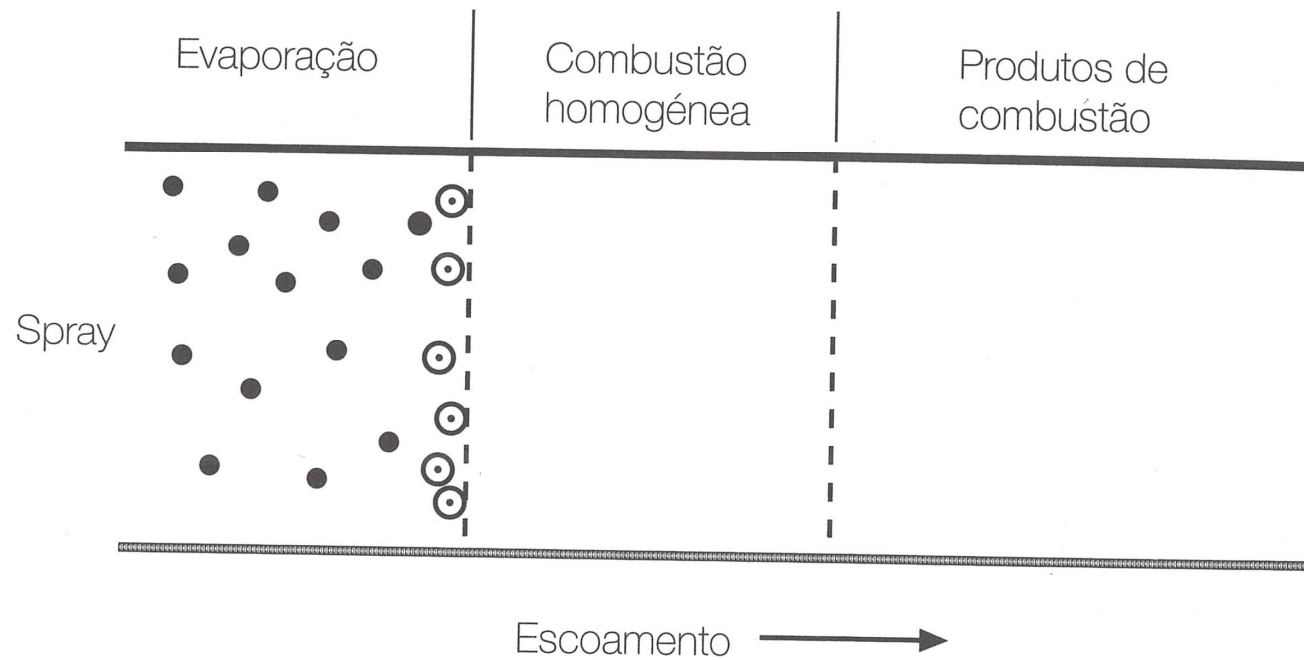
# Combustion of droplets/sprays



Representação esquemática da câmara de combustão de uma turbina a gás.

# Combustion of droplets



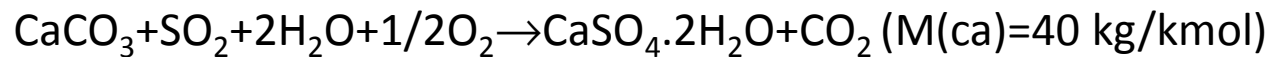


P#18 Mono-dimensional spray Droplets of 200  $\mu\text{m}$ . What should be the length of gas turbine combustion chamber for air and droplet speed of 30 m/s? and the fuel consumption rate?. Assume there is no heat transfer to the droplets interior, and that the droplet is at the boiling point. Air 300 K, 1 bar. Consider two fuels.

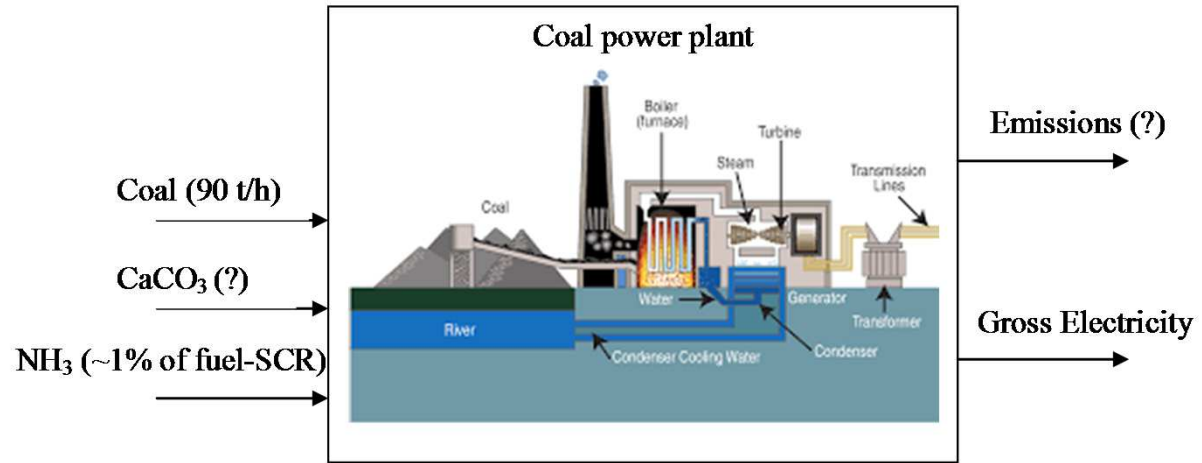
	$T_{\text{flame}}$ (K)	PCI (MJ/kg)
n-hexane (C <sub>6</sub> H <sub>14</sub> )	1700	45.1
Propane (C <sub>3</sub> H <sub>8</sub> )	1900	46.4

Review#2 (exercício 12.4 livro Português) Uma caldeira de uma central termoelétrica é alimentada com um fuel-óleo residual que apresenta a seguinte composição mássica elementar indicada na tabela. Considerando combustão completa com 25% de excesso de ar,

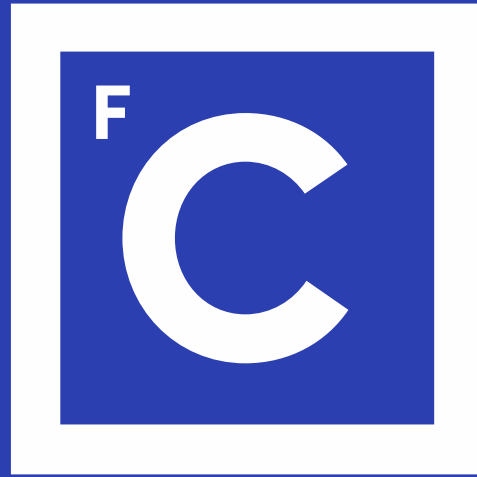
- i) Estime a relação (A/F)<sub>st</sub>.
- ii) Estime a concentração mássica de SO<sub>2</sub> nos produtos de combustão.
- iii) Compare com o limite seco a 3% de O<sub>2</sub> de 200 mg/Nm<sup>3</sup>.
- iv) Pode estimar a concentração de partículas no escape? Como?
- v) Introdução mínima de cal para remoção de S e cumprir limites:



<b>C</b>	<b>86.4%</b>
H	9.8%
N	0.35%
S	1.13%
O	2.28%
Cinzas/Ash	0.04%



**Obrigado**



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